## DIPPR (Design Institute for Physical Property Data) Physical Properties Database

Revised January 2007

This database contains 33 fixed-value properties and 15 temperature-dependent properties of approximately 1793 industrially important compounds. (Accessable only from the presentation computer in the $3^{\text {rd }}$ floor computer room with IP address IP 150.250.102.72. This computer is the one with the phone next to it.)

From the third floor go to link: http://dippr.byu.edu/public/
user: rowanthermo
pswd: che\&dippr
The numeric data in the DIPPR File consist of 29 single value property constants and 15 temperature-dependent properties. Regression equations and coefficients for temperaturedependent properties are also given for calculating additional property values. All of the data are searchable, including Regression Coefficients, percent error, and minimum/maximum temperature values.

If experimental data are not available, values are estimated when possible. Temperaturedependent correlation coefficients, applicable upper and lower temperature limits, and values computed at these limits are included for temperature-dependent properties.

Properties Included (1793 commercially important chemicals and substances):
Temperature Dependent Properties

| Property | DIPPR <br> ID | Units |
| :--- | :---: | :---: |
| Heat Capacity of Ideal Gas | ICP | $\mathrm{J} /(\mathrm{kmol} \cdot \mathrm{K})$ |
| Heat Capacity of Liquid | LCP | $\mathrm{J} /(\mathrm{kmol} \cdot \mathrm{K})$ |
| Heat Capacity of Solid | HVP | $\mathrm{J} /(\mathrm{kmol} \cdot \mathrm{K})$ |
| Heat of Vaporization | LDN | $\mathrm{Jmol} / \mathrm{kmol}$ |
| Liquid Density | SVR | $\mathrm{m}^{3} / \mathrm{kmol}$ |
| Second Virial Coefficient | SDN | $\mathrm{kmol} / \mathrm{m}^{3}$ |
| Solid Density | ST | $\mathrm{N} / \mathrm{m}$ |
| Surface Tension | LTC | $\mathrm{W} /(\mathrm{m} \cdot \mathrm{K})$ |
| Thermal Conductivity of Liquid | STC | $\mathrm{W} /(\mathrm{m} \cdot \mathrm{K})$ |
| Thermal Conductivity of Solid | VTC | $\mathrm{W} /(\mathrm{m} \cdot \mathrm{K})$ |
| Thermal Conductivity of Vapor | VP | Pa |
| Vapor Pressure of Liquid | SVP | Pa |
| Vapor Pressure of Solid or Sublimation Pressure | LVS | $\mathrm{Pa} \cdot \mathrm{s}$ |
| Viscosity of Liquid |  |  |


| Viscosity of Vapor | VVS | $\mathrm{Pa} \cdot \mathrm{s}$ |
| :--- | :---: | :---: |


| Constant Property | DIPPR ID | Units |
| :---: | :---: | :---: |
| Acentric Factor | ACEN | --- |
| Auto Ignition Temperature | AIT | K |
| Dipole Moment | DM | C•m |
| Absolute Entropy of Ideal Gas at 298.15 K and 1 bar | ENT | $\mathrm{J} /(\mathrm{kmol} \cdot \mathrm{K})$ |
| Lower Flammability Limit Temperature | FLTL | K |
| Upper Flammability Limit Temperature | FLTU | K |
| Lower Flammability Limit Percent | FLVL | Vol \% in air |
| Upper Flammability Limit Percent | FLVU | Vol \% in air |
| Flash Point | FP | K |
| Gibbs Energy of Formation for Ideal Gas at 298.15 K and 1 bar | GFOR | J/kmol |
| Standard State Gibbs Energy of Formation at 298.15 K and 1 bar | GSTD | J/kmol |
| Net Standard State Enthalpy of Combustion at 298.15 K | HCOM | $\mathrm{J} / \mathrm{kmol}$ |
| Enthalpy of Formation for Ideal Gas at 298.15 K | HFOR | J/kmol |
| Enthalpy of Fusion at Melting Point | HFUS | $\mathrm{J} / \mathrm{kmol}$ |
| Standard State Enthalpy of Formation at 298.15 K and 1 bar | HSTD | J/kmol |
| Heat of Sublimation | HSUB | $\mathrm{J} / \mathrm{kmol}$ |
| Liquid Molar Volume at 298.15 K | LVOL | $\mathrm{m}^{3} / \mathrm{kmol}$ |
| Melting Point at 1 atm | MP | K |
| Molecular Weight | MW | $\mathrm{kg} / \mathrm{kmol}$ |
| Normal Boiling Point | NBP | K |
| Parachor | PAR | --- |
| Critical Pressure | PC | Pa |
| Radius of Gyration | RG | m |
| Refractive Index | RI | --- |
| Solubility Parameter at 298.15 K | SOLP | $\left(\mathrm{J} / \mathrm{m}^{3}\right)^{1 / 2}$ |
| Standard State Absolute Entropy at 298.15 K and 1 bar | SSTD | $\mathrm{J} /(\mathrm{kmol} \cdot \mathrm{K})$ |
| Critical Temperature | TC | K |
| Triple Point Pressure | TPP | Pa |
| Triple Point Temperature | TPT | K |
| Critical Volume | VC | $\mathrm{m}^{3} / \mathrm{kmol}$ |
| van der Waals Area | VDWA | $\mathrm{m}^{2} / \mathrm{kmol}$ |
| van der Waals Reduced Volume | VDWV | $\mathrm{m}^{3} / \mathrm{kmol}$ |


| Critical Compressibility Factor | ZC | --- |
| :--- | :---: | :---: |

Integrating DIPPR Heat Capacities
Ideal Gas Heat Capacity is given as:

$$
\begin{aligned}
& C_{p i}=A+B\left[\frac{C / T}{\sinh (C / T)}\right]^{2}+D\left[\frac{E / T}{\cosh (E / T)}\right]^{2} \text { with T in Kelvin and } \mathrm{Cp}[=] \mathrm{J} / \mathrm{kmol} * \mathrm{~K} \\
& \Delta H=\int C_{p} \mathrm{~d} T=A \Delta T+B C\left[\operatorname{coth}\left(C / T_{2}\right)-\operatorname{coth}\left(C / T_{1}\right)\right]-D E\left[\tanh \left(E / T_{2}\right)-\tanh \left(E / T_{1}\right)\right]
\end{aligned}
$$

Remember that the enthalpy of a gas is calculated from its standard state enthalpy (See equation 8-19 in Fogler $4^{\text {th }}$ ed. on page 482.)

Below is an example of calculating heat capacities and average heat capacities using DIPPR values for oxygen.

## Oxygen Heat Capacities Values

 The table below gives a summary of the constant property values that are independent of temperature. You will need the Ideal Gas Heat of Formation for an enthalpy calculation.Address eet http://dippr.byu.edu/public/chemsearch.asp?Mode=Printout1\&ChemID=901

| Chemical Database |  |  |  | UNITS | (tampatire | (\%) |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Property Constants |  |  |  | New search | LiNKS | feedback |
| Chemical Abstracts Name:oxygen <br> IUPAC Name:oxygen <br> Synonym: refrigerant 732 <br> Chernical Abstracts Number*: 7782-447 |  |  |  |  | Structural |  |
| Property <br> (click property name for references and data) | Units | Value | Note | Quality Code |  |  |
|  |  |  |  | Data type | Reliability | Source type |
| Molecular Weight Critical Temperature Critical Pressure Critical Volume Crit Compress Factor | $\begin{gathered} \mathrm{kg} / \mathrm{kmol} \\ \mathrm{~K} \\ \mathrm{~Pa} \\ \mathrm{~m} \mathrm{~m}^{n} / \mathrm{kmol} \\ \text { unitless } \end{gathered}$ | 31.9988 154.58 $5.04300 \mathrm{E}+06$ $7.34000 \mathrm{E}-02$ 0.288 |  | Experimental <br> Experimental <br> Experimental <br> Defined | $\begin{aligned} & <3 \% \\ & <5 \% \\ & <10 \% \\ & \text { None } \end{aligned}$ | Evaluated <br> Evaluated <br> Evaluated <br> Staff |
| Melting Point Triple Pt Temperature Triple Pt Pressure Normal Boiling Point Liq Molar Volume | $\begin{gathered} \mathrm{K} \\ \mathrm{~K} \\ \mathrm{~Pa} \\ \mathrm{~K} \\ \mathrm{~m}^{\wedge} 3 / \mathrm{kmol} \end{gathered}$ | $\begin{gathered} 54.361 \\ 54.361 \\ 150 \\ 90.188 \\ 2.80225 \mathrm{E}-02 \end{gathered}$ | $\underline{1}$ | Experimental <br> Experimental <br> Experimental <br> Experimental <br> Experimental | $\begin{aligned} & <1 \% \\ & <1 \% \\ & <3 \% \\ & <1 \% \\ & <1 \% \end{aligned}$ | Evaluated <br> Evaluated <br> Evaluated <br> Evaluated <br> Staff |
| IG Heat of Formation IG Gibbs of Formation IG Absolute Entropy Std Heat of Formation Std Gibbs of Formation | J/kmol <br> J/kmol <br> J/kmol*K <br> J/knol <br> J/kmol | 0.0 <br> 0.0 <br> $2.05043 \mathrm{E}+05$ <br> 0.0 <br> 0.0 | $\underline{3}$ | Experimental <br> Defined | $<0.2 \%$ <br> Unknown | Evaluated <br> Staff |
| Std Absolute Entropy Heat Fusion at Melt Pt Std Net Heat of Comb Acentric Factor Radius of Gyration | J/kmol*K <br> J/kmol <br> J/kmol <br> unitless <br> Ill | $\begin{gathered} 2.05043 \mathrm{E}+05 \\ 4.44000 \mathrm{E}+05 \\ 0.0 \\ 2.21798 \mathrm{E}-02 \\ 6.80000 \mathrm{E}-11 \end{gathered}$ |  | Experimental Experimental <br> Defined <br> Defined | $\begin{aligned} & <0.2 \% \\ & <3 \% \\ & \text { None } \\ & <3 \% \end{aligned}$ | Evaluated Evaluated <br> Staff <br> Staff |
| Solubility Parameter Dipole Moment van der Waals Volume yan der Waals Area Refractive Index | $\begin{gathered} \left(\mathrm{J} / \mathrm{m}^{\wedge} \mathrm{c}^{*}\right)^{\wedge} 0.5 \\ \mathrm{~m}{ }^{\wedge} 3 / \mathrm{kmol} \\ \mathrm{~m}^{2} 2 \\ \text { unitless } \end{gathered}$ | $\begin{gathered} 8.18200 \mathrm{E}+03 \\ 0.0 \\ 1.30000 \mathrm{E}-02 \\ 2.35000 \mathrm{E}+08 \\ 1.221 \end{gathered}$ | $\begin{aligned} & \underline{4} \\ & \underline{5} \\ & \underline{5} \end{aligned}$ | Defined <br> Defined <br> Defined <br> Experimental | $\begin{gathered} \text { None } \\ <3 \% \\ <5 \% \\ \text { Unknown } \end{gathered}$ | Staff Staff Staff Evaluated |
| Flash Point <br> Lower Flammability Limit <br> Upper Flammability Linnit <br> Lower F Fammm Limit Temp <br> Upper Flamm Linit Temp |  |  | $\begin{aligned} & \hline \frac{7}{7} \\ & \frac{7}{7} \end{aligned}$ |  |  |  |
| Auto Ignition Temp Parachor <br> Heat of Sublimation Dielectric Constant | K unitless J/kmol unitless |  | 7 |  |  |  |
| Issue Date: 7/1/1981 <br> Notes: <br> 1. Triple point temper <br> 2. Determined at the <br> 3. Calculated from th standard state abs <br> 4. For the hypothetic | ure. <br> mal boiling p tandard state ate entropy. iquid at 298 | thalpy of form $101325 \mathrm{~Pa} .$ | ion and | Revision D <br> the | : 81/1994 |  |

Below is the page showing the temperature Dependent properties.

| Address http://dippr.byu.edu/public/chemsearch.asp?M Mode=Printout2\&ChemID=901 |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Chemical Database Temperature-Dependent Properties |  |  | UNITS |  |  |  |
| Chemical Abstracts Name: oxygen |  | $\begin{array}{r} \mathrm{O}_{2} \\ \text { oxygen } \end{array}$ |  |  |  |  |
| Property (click property name for references and data sets) | NoteEquation \#Quality | Coefficients |  |  |  |  |
|  |  | A | B | C | D | E |
| Solid Density <br> Min: $(20.65,4.4552 \mathrm{E}+01)$ <br> Max: $(20.65,4.4552 \mathrm{E}+01)$ | $\frac{100}{<25 \%}$ | $4.4552 \mathrm{E}+01$ |  |  |  |  |
| Liquid Density <br> Min: (54.35, 4.0770E+01) <br> Max: $(154.58,1.3605 \mathrm{E}+01)$ | $\frac{105}{<1 \%}$ | $3.9143 \mathrm{E}+00$ | 2.8772E-01 | $1.5458 \mathrm{E}+02$ | $2.9240 \mathrm{E}-01$ |  |
| Solid Vapor Pressure | $\underline{1}$ |  |  |  |  |  |
| Vapor Pressure <br> Min: $(54.36,1.4754 \mathrm{E}+02)$ <br> Max: $(154.58,5.0206 \mathrm{E}+00)$ | $\frac{101}{<1 \%}$ | 5.1245E+01 | $-1.2002 \mathrm{E}+03$ | $-6.4361 \mathrm{E}+00$ | $2.8405 \mathrm{E}-02$ | $1.0000 \mathrm{E}+00$ |
| Heat of Vaporization <br> Min: $(54.36,7.7419 \mathrm{E}+06)$ <br> Max: (154.58,0.0) | $\begin{gathered} \frac{2}{206} \\ \frac{106}{1 \%} \end{gathered}$ | $9.0080 \mathrm{E}+06$ | 4.5420E-01 | -4.0960E-01 | 3.1830E-01 |  |
| Solid Heat Capacity Min: $(13.46,4.7613 \mathrm{E}+03)$ Max: $(43.78,4.6573 \mathrm{E}+04)$ | $\frac{100}{<5 \%}$ | -1.3800E+04 | $1.3790 \mathrm{E}+03$ |  |  |  |
| Liquid Heat Capacity <br> Min: $(54.36,5.3646 \mathrm{E}+04)$ <br> Max: (142,9.0662E+04) | $\frac{100}{<3 \%}$ | $1.7543 \mathrm{E}+05$ | -6.1523E+03 | $1.1392 \mathrm{E}+02$ | -9.2382E-01 | $2.7963 \mathrm{E}-03$ |
| Ideal Gas Heat Capacity <br> Min: $(50,2.9103 \mathrm{E}+04)$ <br> Max: (1500, 3.6533E+04) | $\frac{107}{<1 \%}$ | $2.9103 \mathrm{E}+04$ | $1.0040 \mathrm{E}+04$ | $2.5265 \mathrm{E}+03$ | $9.3560 \mathrm{E}+03$ | $1.1538 \mathrm{E}+03$ |
| Second Virial Coefficient <br> Min: (77.29,-3.3311E-01) <br> Max: (772.9, 1.9176E-02) | $\frac{104}{<5 \%}$ | 3.9840E-02 | $-1.5840 \mathrm{E}+01$ | -7.8300E+04 | $4.6000 \mathrm{E}+13$ | $-3.4000 \mathrm{E}+15$ |
| Liquid Viscosity <br> Min: $(54.36,7.1704 \mathrm{E}-04)$ <br> Max: $(150,6.9896 \mathrm{E}-05)$ | $\frac{101}{<25 \%}$ | -4.1476E+00 | $9.4040 \mathrm{E}+01$ | $-1.2070 \mathrm{E}+00$ |  |  |
| Vapor Viscosity Min: $(54.35,3.7725 \mathrm{E}-06)$ Max: $(1500,6.3705 \mathrm{E}-05)$ | $\frac{102}{<5 \%}$ | 1.1010E-06 | 5.6340E-01 | $9.6300 \mathrm{E}+01$ |  |  |
| Solid Thermal Conductivity | $\underline{1}$ |  |  |  |  |  |
| Liq Thermal Conductivity <br> Min: $(60,1.9130 \mathrm{E}-01)$ <br> Max: $(150,6.7100 \mathrm{E}-02)$ | $\frac{100}{<5 \%}$ | 2.7410E-01 | -1.3800E-03 |  |  |  |
| Vap Thermal Conductivity <br> Min: $(80,6.9091 \mathrm{E}-03)$ <br> Max: (2000, 1.2655E-01) | $\frac{102}{<10 \%}$ | 4.4994E-04 | $7.4560 \mathrm{E}-01$ | $5.6699 \mathrm{E}+01$ |  |  |
| Surface Tension Min: $(54.35,2.2500 \mathrm{E}-02)$ Max: $(154.58,0.0)$ | $\frac{106}{<3 \%}$ | $3.8066 \mathrm{E}-02$ | $1.2136 \mathrm{E}+00$ |  |  |  |
| Issue Date:7/1/1981 <br> Notes: <br> 1. No experimental val <br> 2. Data calculated fron | satisfactory eyron equati | rediction meth used in regr | available. sion. | $\text { sion Date: } 8 / 1$ | $1992$ |  |

http://dippr.byu.edu/public/chemsearch.asp?Mode=Reference\&Che $\underline{\mathrm{mID}=901 \& \text { Property }=\mathrm{ICP}}$

From the Property Calculator:



| 2987. TRC Thermodynamic TablesHydrocarbons; Thermodynamics Research Center, The Texas A\&M University System, College Station, TX, 1985. |  |
| :---: | :---: |
| Temperature (K) | Ideal Gas Heat Capacity ( $\mathrm{J} / \mathrm{kmol} * \mathrm{~K}$ ) |
| 50 | $2.91030 \mathrm{E}+04$ |
| 100 | $2.91060 \mathrm{E}+04$ |
| 150 | $2.91090 \mathrm{E}+04$ |
| 200 | $2.91260 \mathrm{E}+04$ |
| 273.16 | $2.92720 \mathrm{E}+04$ |
| 298.15 | $2.93760 \mathrm{E}+04$ |
| 300 | $2.93850 \mathrm{E}+04$ |
| 400 | $3.01060 \mathrm{E}+04$ |
| 500 | $3.10910 \mathrm{E}+04$ |
| 600 | $3.20900 \mathrm{E}+04$ |
| 700 | $3.29810 \mathrm{E}+04$ |
| 800 | 3.37330E+04 |
| 900 | $3.43550 \mathrm{E}+04$ |
| 1000 | $3.48700 \mathrm{E}+04$ |
| 1100 | $3.53000 \mathrm{E}+04$ |
| 1200 | $3.56670 \mathrm{E}+04$ |
| 1300 | $3.59880 \mathrm{E}+04$ |
| 1400 | $3.62770 \mathrm{E}+04$ |
| 1500 | $3.65440 \mathrm{E}+04$ |

Here are the fitted values of Heat Capacity for oxygen gas at temperatures of 300 K and 1000 K . Notice that these are not the average heat capacities for the range of 300 to 1000 K .
$\qquad$

calculate the average heat capacity value from DIPPR constants POLYMATH can be used to numerically integrate - or to check you analytical integration. For Example from the result below the value of the average heat capacity for oxygen from 300 K to 1000 K is $3.235 \times 10^{4}$ $\mathrm{J} /(\mathrm{kmol} \mathrm{K})$. This result can also be obtained from a numerical integration.

$$
\begin{aligned}
C_{p i}= & A+B\left[\frac{C / T}{\sinh (C / T)}\right]^{2}+D\left[\frac{E / T}{\cosh (E / T)}\right]^{2} \text { with T in Kelvin and } C p[=] \mathrm{J} / \mathrm{kmol} * \mathrm{~K} \\
\Delta H= & \int_{300 K}^{1000 K} C_{p} \mathrm{~d} T=A(1000-300)+B C[\operatorname{coth}(C / 1000 K)-\operatorname{coth}(C / 300 K)] \\
& -D E[\tanh (E / 1000 K)-\tanh (E / 300 K)] \\
\bar{C}_{p}= & \frac{\int_{300 K}^{1000 k} C_{p} \mathrm{~d} T}{1000 K-300 K}=3.235 \times 10^{4} \mathrm{~J} /(\mathrm{kmol} \mathrm{~K})
\end{aligned}
$$

This is given as the final value of Cpavg in the POLYMATH program given below.

For a numerical integration Polymath can be used:

Ordinary Differential Equations
Calculated values of DEQ variables

| Variable |  | Initial value | Minimal value | Maximal value | Final value |
| :--- | :--- | :--- | :--- | :--- | :--- |
| 1 | T | 298. | 298. | 1000. | 1000. |
| 2 | H | 0 | 0 | $2.27 \mathrm{E}+07$ | $2.27 \mathrm{E}+07$ |
| 3 | A | $2.91 \mathrm{E}+04$ | $2.91 \mathrm{E}+04$ | $2.91 \mathrm{E}+04$ | $2.91 \mathrm{E}+04$ |
| 4 | B | $1.004 \mathrm{E}+04$ | $1.004 \mathrm{E}+04$ | $1.004 \mathrm{E}+04$ | $1.004 \mathrm{E}+04$ |
| 5 | C | 2526.5 | 2526.5 | 2526.5 | 2526.5 |
| 6 | D | 9356. | 9356. | 9356. | 9356. |
| 7 | E | 1153.8 | 1153.8 | 1153.8 | 1153.8 |
| 8 | Cp | $2.935 \mathrm{E}+04$ | $2.935 \mathrm{E}+04$ | $3.486 \mathrm{E}+04$ | $3.486 \mathrm{E}+04$ |
| 9 | Cpavg | 0 | 0 | $3.235 \mathrm{E}+04$ | $3.235 \mathrm{E}+\mathbf{0 4}$ |

## Differential equations

$1 \mathrm{~d}(\mathrm{H}) / \mathrm{d}(\mathrm{T})=\mathrm{Cp}$

## Explicit equations

$1 \mathrm{~A}=2.9103 \mathrm{e} 4$
$2 B=1.0040 \mathrm{e} 4$
$3 \mathrm{C}=2526.5$
$4 \mathrm{D}=9.3560 \mathrm{e} 3$
$5 \mathrm{E}=1.1538 \mathrm{e} 3$
$6 C p=A+B *(C / T / \sinh (C / T))^{\wedge} 2+D *(E / T / \cosh (E / T))^{\wedge} 2$
7 Cpavg $=\mathrm{H} /(1000-300)$

## General

| Total number of equations | 8 |
| :--- | :--- |
| Number of differential equations | 1 |
| Number of explicit equations | 7 |
| Elapsed time | 0.000 sec |
| Solution method | RKF_45 |
| Step size guess. h | 0.000001 |
| Truncation error tolerance. eps | 0.000001 |

Note you can change the units of your system on this page:


