

MASS TRANSFER COEFF. FOR VARIOUS GEOMETRIES - MASS

TRANSFER INSIDE A TUBE

A TUBE IS COATED ON THE INSIDE WITH NAPHTHALENE AND HAS AN INSIDE DIAM. OF 2.0 CM AND A LENGTH OF 11.0 CM. AIR AT 45°C AND AN AVG. PRESSURE OF 1.0 atm FLOWS THROUGH THE TUBE AT A VELOCITY OF 8.0 cm/s. ASSUMING THAT THE ABSOLUTE PRESSURE REMAINS ESSENTIALLY CONSTANT, CALCULATE THE CONC. OF NAPHTHALENE IN THE EXIT AIR. AIR ENTERING THE TUBE HAS A 0 CONC. OF NAPHTHALENE.

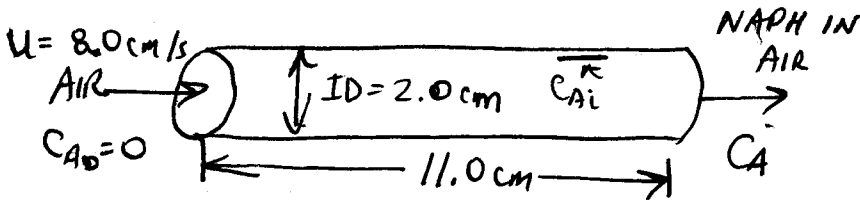
GIVEN: DIFFUSIVITY NAPHTHALENE - AIR = $6.92 \times 10^{-2} \text{ cm}^2/\text{s}$
@ 45°C

GIVEN: VAPOR PRESSURE; NAPHTHALENE IN AIR = 7.31×10^{-4} atm

PROPERTIES: @ $45^\circ\text{C} = 318\text{K}$

$\mu_{\text{AIR}} = 0.0187$ $\varphi = 1.87 \times 10^{-4} \text{ g/cm}\cdot\text{s}$
 VISCOSITY NOMOGRAPH
 OR USE TABLES

$\rho_{\text{AIR}} = \frac{(\text{MW}) \frac{1}{V}} = \frac{P}{RT} (\text{MW}) = \frac{(1 \text{ atm})(29 \text{ g/mol})}{\left(\frac{82.06 \text{ cm}^3 \text{ atm}}{\text{mol K}}\right)(318 \text{ K})}$
 $\rho_{\text{AIR}} = 1.11 \times 10^{-3} \text{ g/cm}^3$
 (OR USE TABLES)



NAPHTHALENE = 'A' (vapor/liquid)
 AIR = 'B' (gas)

$Sc = \frac{\mu}{\rho D_{AB}}$

μ AND ρ ARE PROPERTIES OF 'B'

$Sc = \frac{1.87 \times 10^{-4} \text{ g/cm}\cdot\text{s}}{(1.11 \times 10^{-3} \text{ g/cm}^3)(6.92 \times 10^{-2} \text{ cm}^2/\text{s})} = 2.43$

$$Re = \frac{D u \rho}{\mu}$$

μ, ρ ARE PROPERTIES OF 'B'

D = TUBE DIAM.

$$Re = \frac{(2.0 \text{ cm})(8.0 \text{ cm/s})(1.11 \times 10^{-3} \text{ g/cm}^3)}{(1.87 \times 10^{-4} \text{ g/cm}\cdot\text{s})}$$

$$Re = 94.97 \rightarrow \text{LAMINAR}$$

$$\frac{C_A - C_{A0}}{C_{Ai} - C_{A0}} = 5.5 \left(Re \text{ Sc } \frac{D}{L} \frac{\pi}{4} \right)^{-2/3}$$

$$\frac{C_A - C_{A0}}{C_{Ai} - C_{A0}} = 5.5 \left[(94.97)(2.43) \left(\frac{2.0}{11.0} \right) \left(\frac{\pi}{4} \right) \right]^{-2/3}$$

$$= 0.5350$$

AT G-L INTERFACE, C_{Ai} , IS THE VAPOR

PRESSURE OF NAPH. IN AIR = ~~0.73 atm~~

Liq. Nap
↓
Nap. as vapor
Air

$$C_{Ai} = \frac{n}{V} = \frac{P_{Ai}}{RT} = \frac{7.31 \times 10^{-4} \text{ atm}}{\left(\frac{82.06 \text{ cm}^3 \text{ atm}}{\text{mol K}} \right) (318 \text{ K})}$$

$$C_{Ai} = 2.80 \times 10^{-8} \frac{\text{mol}}{\text{cm}^3}$$

$$\frac{C_A - C_{A0}}{C_{Ai} - C_{A0}} = \frac{C_A - 0}{2.80 \times 10^{-8} - 0} = 0.5350$$

$$C_A = 1.50 \times 10^{-8} \frac{\text{mol}}{\text{cm}^3}$$